



WEBINAR ON HIGH TEMPERATURE HEAT PUMPS

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Case study Cremo: Integration concept and status

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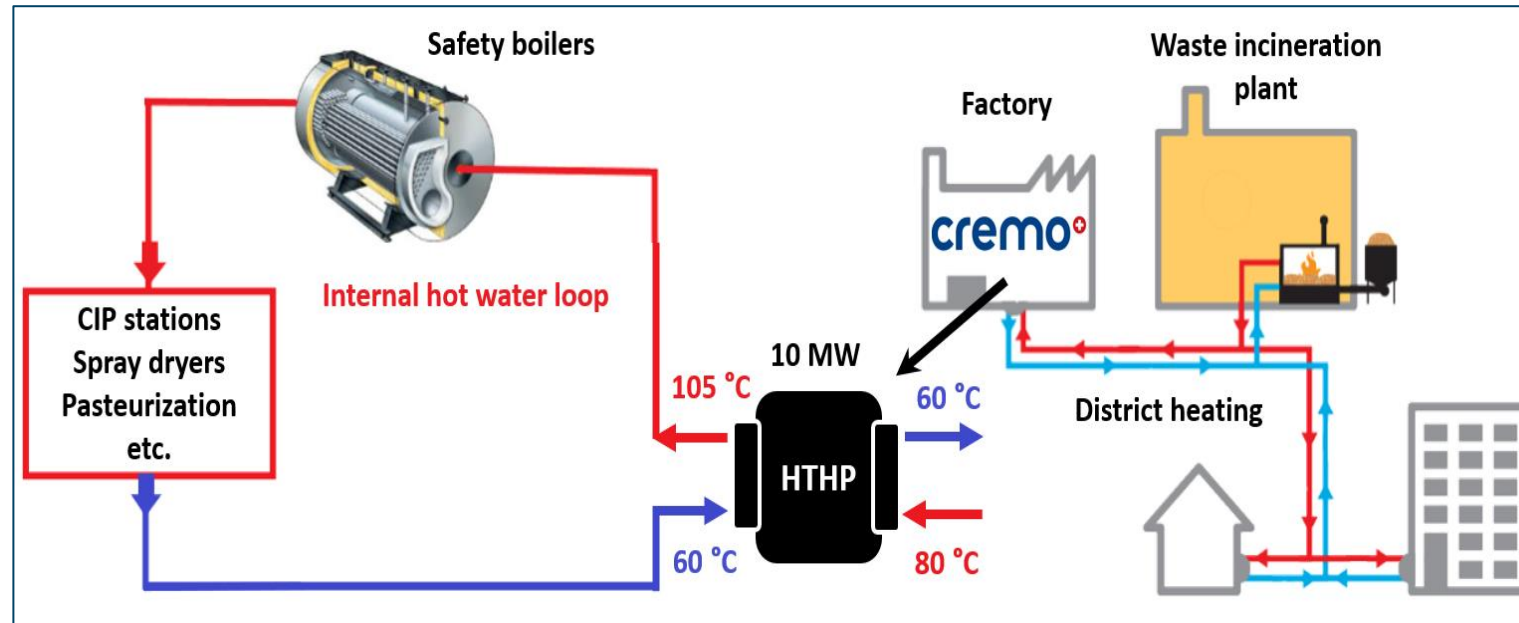
Company presentation

- Among largest milk processing companies in Switzerland (est. 1927) owned at 90% by milk producers
- 8 production sites in Switzerland
- Villars-sur-Glâne factory processes 240'000 t/yr of milk to produce
 - Cheese and butter
 - Skim milk, whey and milk permeate powder



Potential opportunities for HTHP

- Steam for milk permeate powder drying plant
- Boost district heating network distribution temperature
- Upgrade heat recovered in the factory to a hot water loop



Selected case study for HTHP

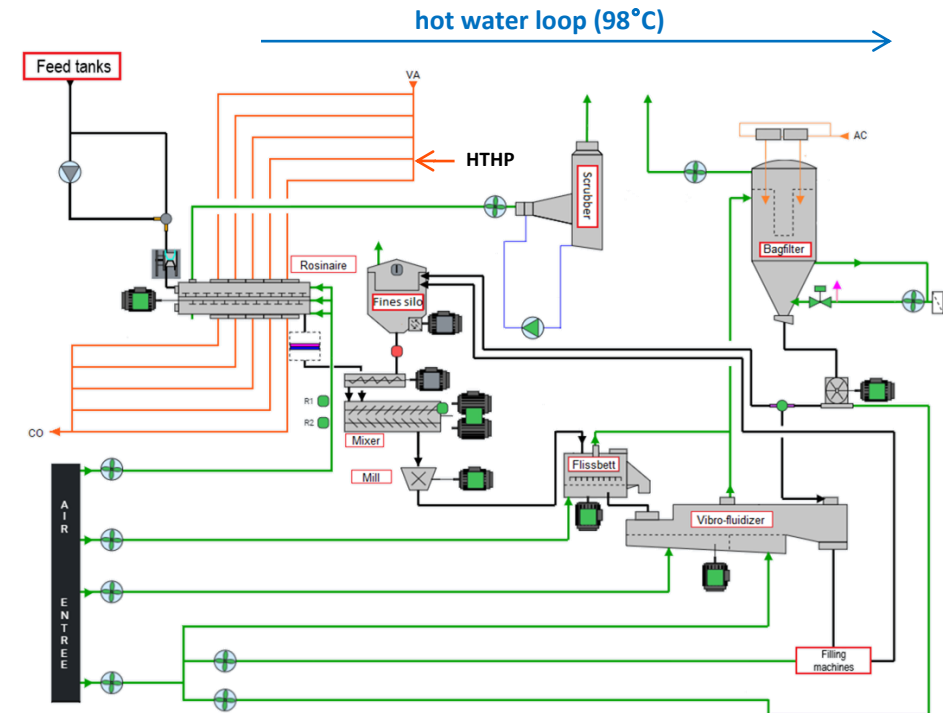
- Supply steam to the milk permeate powder drying process
 - Low pressure steam needed
 - 15% of factory steam consumption (from gas boiler)
 - Simultaneity and proximity of sources & sinks (semi-continuous process)
 - Potential waste heat to be recovered



Characterisation of the streams

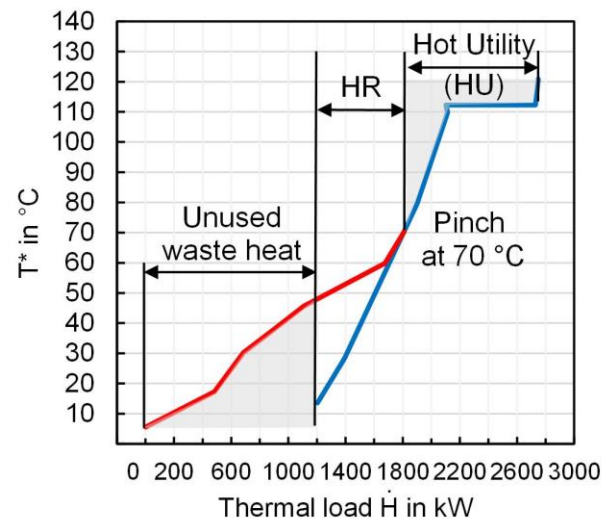
- Measurement campaign : fundamental needs vs current heat supply?

- Sinks :
 - Steam for paddle dryer (1.8 bara steam)
 - Air heaters for paddle dryer, static & fluidized bed (between 75°C - 117°C)
- Sources :
 - Exhaust air from paddle dryer and from static & fluidized bed (66°C)
 - Hot water loop (98°C)

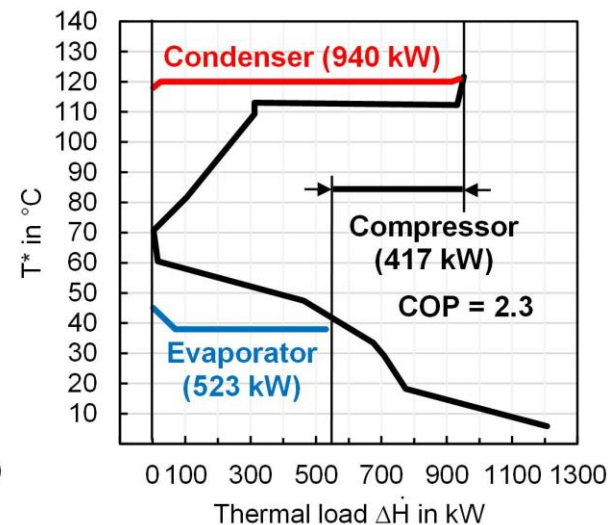


Pinch Analysis of case study

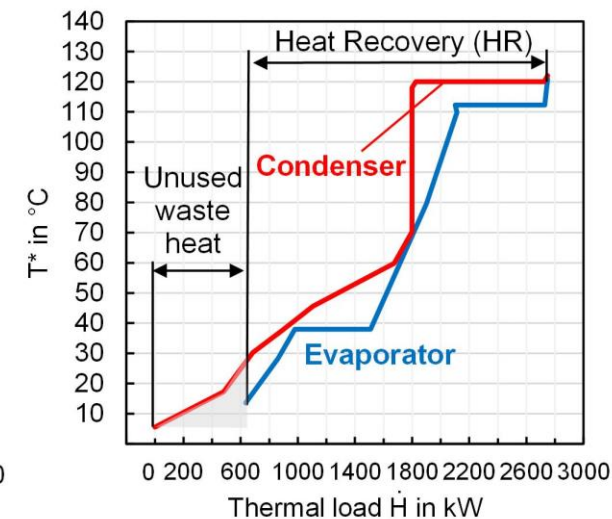
- Heat recovery potential through direct heat transfer of about 600 kW between air flows
- HTHP integration identified providing low-pressure steam at 110 °C using humid exhaust air as a heat source
 - HTHP : evaporation at 38 °C, condensation at 120 °C → low expected COP of 2.3
 - Constrains : existing heat recovery on exhaust air streams / very little space in air heating room for modifications



Composite curves (CC)



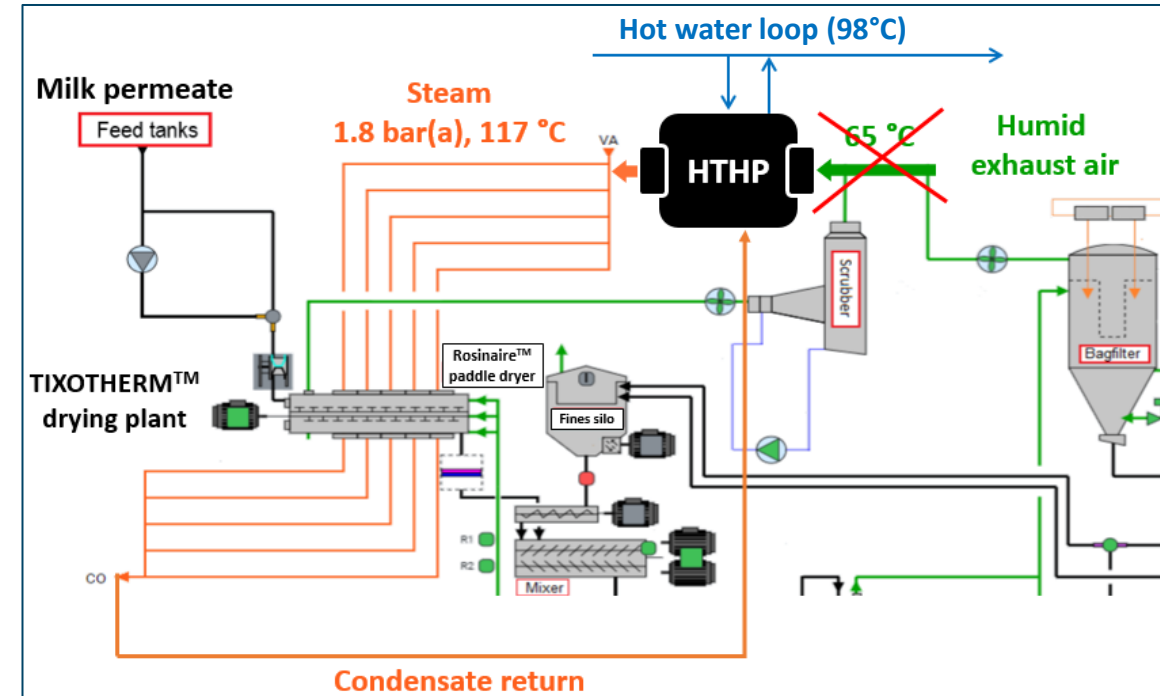
Grand composite curves (GCC)



Composite curves with HP integration

Integration concepts

- *Optimal integration from Pinch analysis*
 - *Heavy modifications required to existing heat recovery system*
 - *Spatial restrictions*
- **Considered concept**
 - **Sink : 810 kg/h steam at 1.8 bar(a) for the paddle dryer**
 - **Source : 98°C water loop**
- *Alternative concept tried*
 - *Sink : 1'300 kg/h at 4 bar(a) for paddle dryer + air heaters*
 - *Source : 98°C water loop*
 - *Proved to be a technical no-go with MVR*



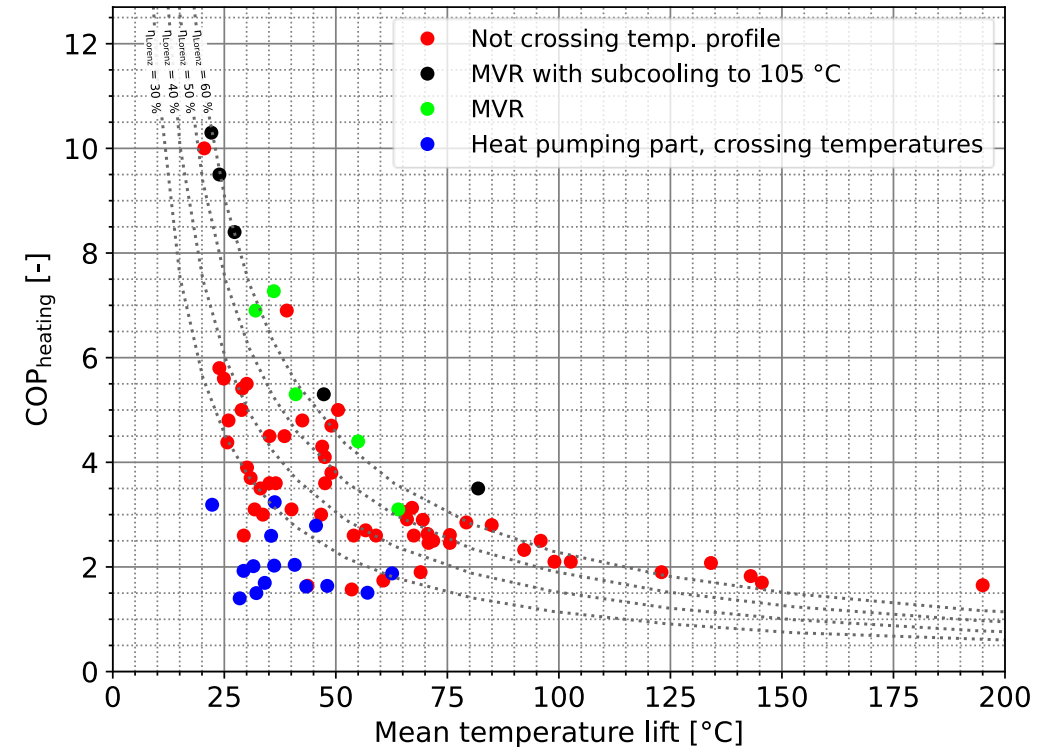
Integration considerations

- Points to be checked
 - Simultaneity sink-source?
 - Heat storage needed?
 - Space available?
 - Supporting structure sufficient?
 - Electrical power reinforcement needed?
 - Compliance to hygienic conditions for all equipment?
 - Introduction of equipment?
 - Redundancy?



Preliminary evaluation

- Initial data and hypothesis
 - 1.8 bar(a) / 500 kW steam produced
 - MVR heat pump with COP of 9
 - Annual operating time 2700h/yr
 - Specific HTHP cost 450 CHF/kW
 - Subsidies from myclimate & SFOE
- First result estimates
 - Annual energy saving : 15%
 - Annual CO₂ emissions reduction : 94%
 - Payback of 4 years



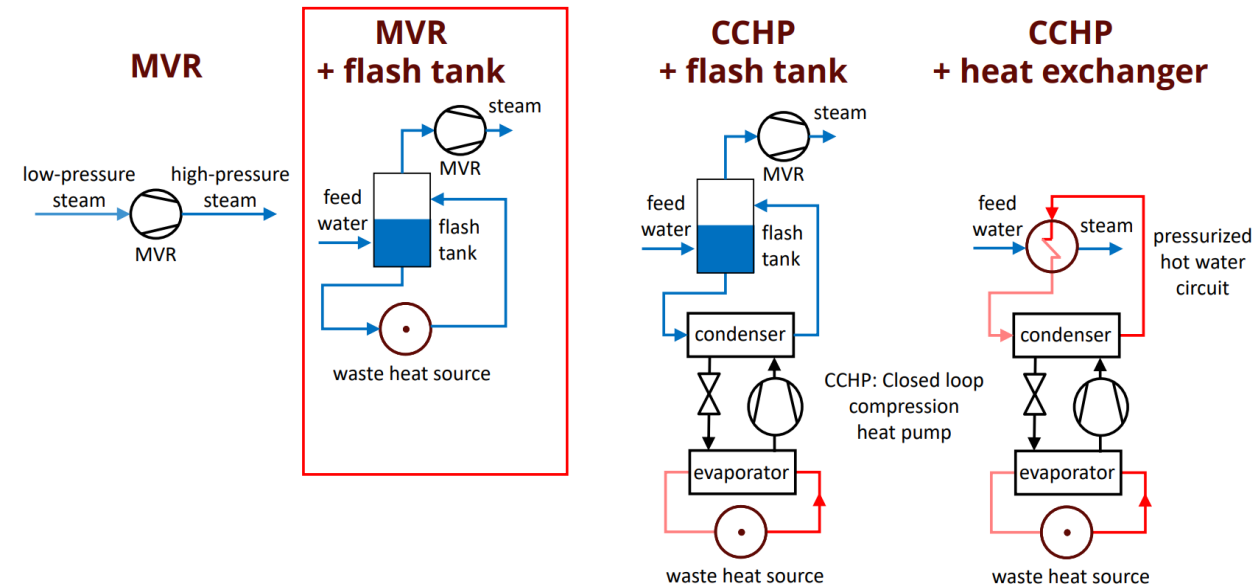
[IEA Annex 58 Task 1, based on manufacturer data]

Heat pump type selection

- Various steam-generating HP technologies available

- MVR technology chosen

- Mature and reliable technology
- Good efficiency
- Contains no refrigerant fluid
- Sub-atmospheric evaporation



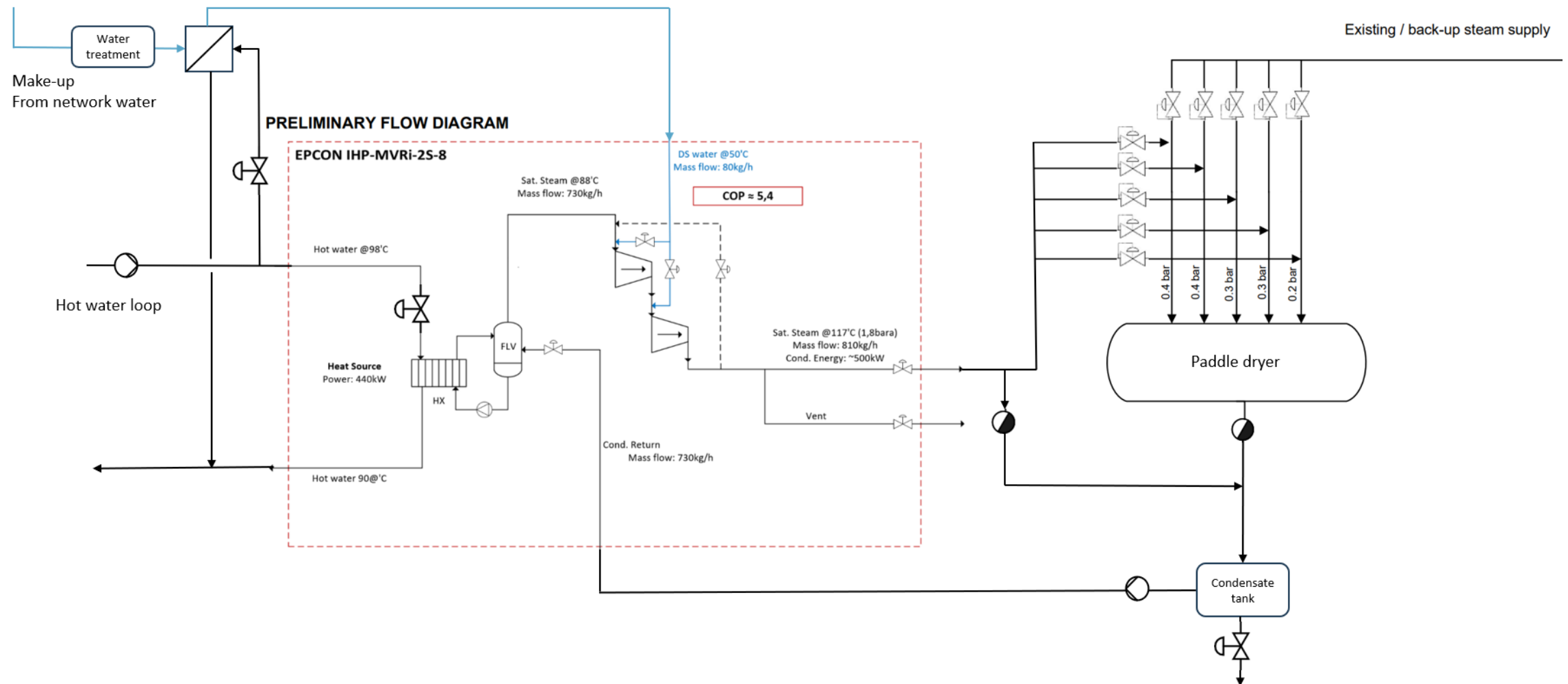
- Challenges faced

- Small capacity out of the specification for various suppliers
- Introduction to 5th floor by the freight lift (→ setup on 2 skids)

Source : IEA Annex 58

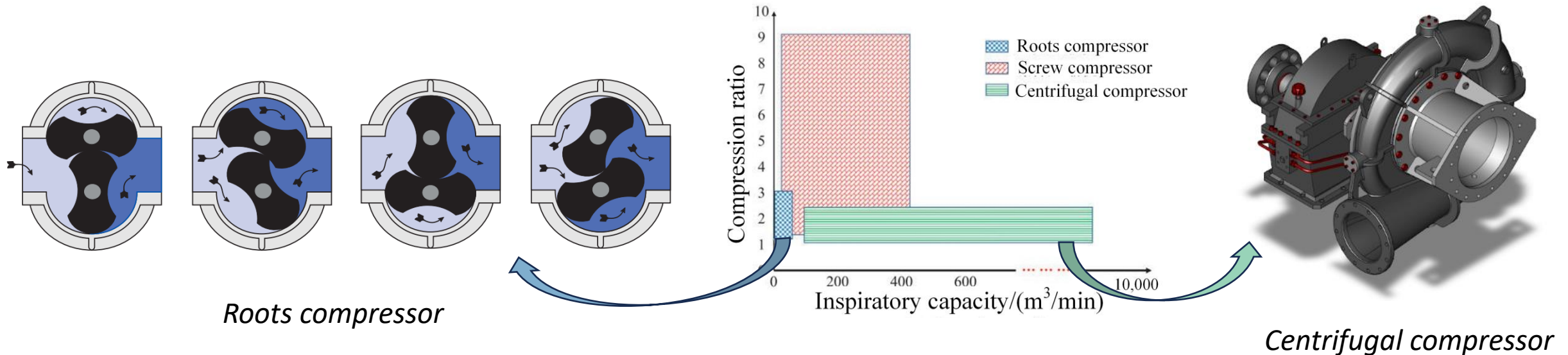
Integration scheme

- EPCON MVR-HTHP integration concept at Cremo factory : technically feasible



Performance gap

- Expected COP = 9 for MVR-HP → COP = 5.4 effective value
- Low steam flowrate
 - Compression technology affected
 - 40-60% isentropic efficiency of roots compressor vs 70-90% of centrifugal blower
- Better efficiency for large scale compressors in general



Project results

- Total cost of the project (CAPEX)
 - CHF 1'570'700.-
- Specific cost
 - 3'140 CHF/kW installed
- Cost efficiency
 - OPEX overcost : 72 CHF/tCO₂ avoided
 - No profitability
 - 22yrs payback if 200CHF/tCO₂ conceded for avoided emissions
 - Heat source not free
 - High specific cost of HTHP
 - Lower COP than expected
 - Moderate operating time
 - Not eligible to myclimate subsidies, to be confirmed for SwissEnergy program (included here)

Project costs breakdown	
Source side	4.5 %
MVR HTHP incl. delivery & installation	85.0%
Secondary side	6.5 %
Other	4.0%

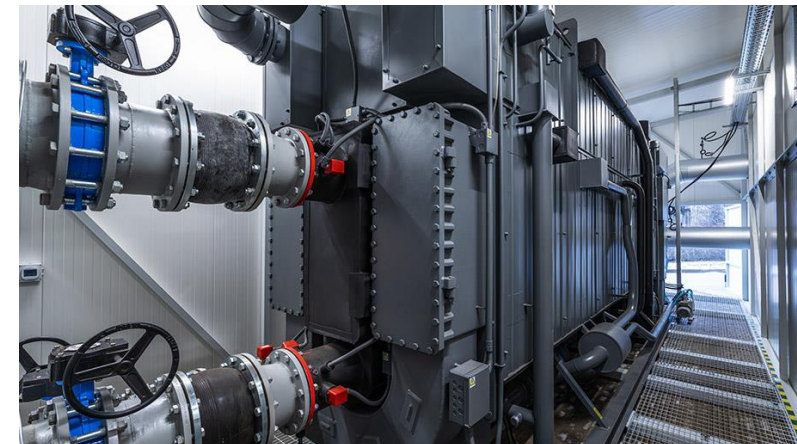
Environmental benefits	
Annual energy saving	15%
Annual CO ₂ emissions reduction	98%

Cost efficiency improvement

- Alternative heat source, broaden the search out of particular process
 - Waste heat (under study)
 - Even better if cooling utility avoided by HTHP integration
- Larger heat pump
 - Lower specific cost
 - Increased efficiency
- Increased operating time
- Higher cost for gas

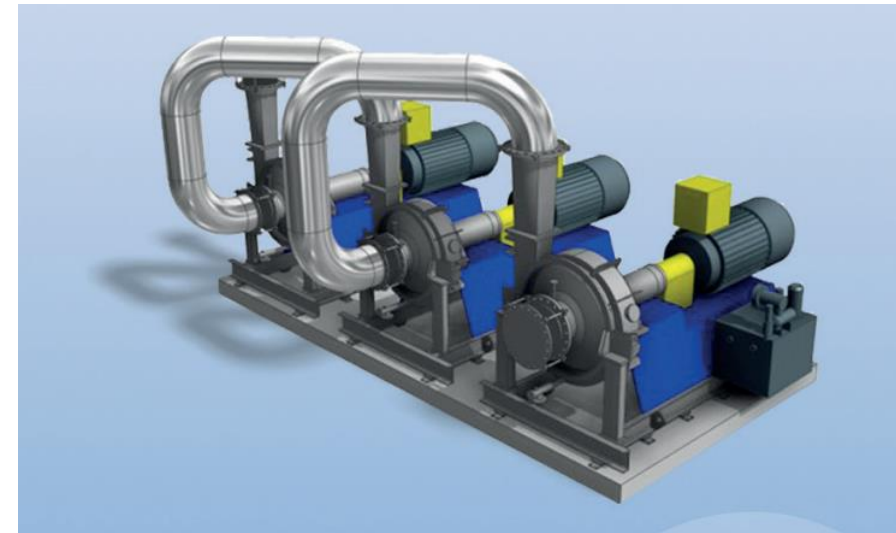
Subsidy programs

- HP for process heat – SwissEnergy/SFOE
 - Subsidy of max. 40% of over-cost for industrial heat HP project
- Industrial HP - Myclimate
 - Subsidy
 - Global amount of 18 ct/kWh (average over last 3 years consumption)
 - Yearly payment of CHF 160.-/tCO₂ up to subsidy amount is reached
 - Subsidy agreement until end of 2030
- Check the eligibility conditions



Conclusions

- Technically feasible solution found
- Benefits
 - Environmental : 98% annual CO₂ emissions reduction for the paddle dryer steam supply
 - Considered MVR-HP contains no refrigerant fluid
 - Installation close to the process unit keeps integration costs down
 - Efficiency : production as close as possible to the fundamental heating needs
 - Source : hot water loop availability
- Challenges
 - Profitability to replace fossil steam production
 - Low steam flow rate for MVR technology
 - Performance gap with larger machines
 - Increased price CHF/kWh for HTHP
 - Lack of data to find sufficient waste heat at interesting temperature
 - Semi-continuous production with moderate operating time
 - Factory building : access to the 5th floor for HP introduction



- Further information on HTHP : <https://heatpumpingtechnologies.org/annex58>